(b) oxidizing the seawater after the gas-liquid contact with air in an oxidation apparatus, and

(c) mixing raw seawater with the oxidized seawater, whereby the exhaust gas and the oxidized seawater are discharged, without using chemicals, to the ocean, wherein the seawater is introduced into a gas-liquid contact apparatus including an absorption column having a column diameter of at least one perforated plate having an free-space ration Fc of 0.25 to 0.5 and packed with at least one type of packing material to a packing height of 0.5m to 4m, in such an amount that a ratio L/G of the flow rate L ($kg/m^2 \cdot hr$) of the seawater to the flow rate G ($kg/m^2 \cdot hr$) of the gas to be treated from the top of the column is at least 3.6 and a flow rate L of the seawater is 1×10^4 to 25×10^4 $kg/M^2 \cdot hr$ and introducing a treated gas in such an amount that a range of a superficial gas velocity Ug in the apparatus from the bottom of the gas-liquid contact apparatus is less than 2 Ugm (m/sec);

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$$Ugm = 49.14\ Fc^{G.7}(\rho_G/\rho_L \times 10^{-3})^{-0.5} \cdot (L/G)^{-1/3} \cdot \sqrt{g \cdot L}$$

wherein L is a capillary constant $\sqrt{2\sigma / \rho^L \cdot g}$

g is a gravitational acceleration (m/sec^2), and

o is a surface tension of seawater (kg/sec^2)

in the case of using a perforated or grid plate column without weir and downcomer composed of at least one perforated plate and the ratio ρ_G/ρ_L of the density ρ^G (kg/m^3) of the treated gas to the density ρ_L (kg/m^3) of seawater is at least 0.838×10^{-3}.

2. (Twice Amended) A method as claimed in claim 1, wherein the free-space ratio Fc is 0.3 to 0.4 and the ratio L/G is 7 to 25.

SubCT